

Carbon dioxide absorption through ceramic membrane in different waterdifferent water

Abstract

An attempt has been made to assess t The efficiency of clay alumina based ceramic membrane for the absorption of Carbon \underline{Pd} ioxide (Co₂) in various types of water was investigated. The dissolutions of Co₂carbon dioxide are observed for three different types of water – tap waterand simulated water of Central Glass and Ceramic Research Institute (CGCRI) Kolkata, and simulated sea water prepared in the CGCRI laboratory and milli-Q water (resistance of 18.2 Ω). The absorption of Co₂Carbon Dioxide absorption set up was with porous tubular ceramic membrane module having a contact surface area 6329.86 mm² is used for the experiment. The objective of this work is to present experimental data that would show absorption efficiencies of different types of the above mentioned three different types of water, their compositions after absorption, physical and chemical nature, the effect of temperature, rate of dissolution, and pH₂-ete.

Key words, CO2 dissolution, absorption, membrane, membrane contactor, Henry's law, natural water

Introduction

- Due to the industrial revolution, there is a continuous emission and absorption of greenhouse gases in the atmosphere which resulted in – Global warming or the continual and significant rise in the average temperature of the earth¹², is mainly caused by the emission of greenhouse gases into the atmosphere.⁴ The greenhouse gases absorb and radiate harmful infrared rays and radiate them into the atmosphere, increasing the earth's temperature by significant amount² Co₂ was found to be Θ_0 ne of the most hazardous greenhouse gases on the earth's atmosphere is Carbon Dioxide. The emission of Carbon Dioxide into the earth's atmosphere has increased manifold over the past three decades because of the industrial revolution. It is estimated that the concentration of Carbon Dioxide which has increased from 290 ppm in 1900 to about 400 ppm at present.³ Approximately 60% of Global emissions of gas was due to Co₂ Carbon Dioxide gas contributes to more than 60% of global emissions because of the large of gas that is produced.⁴ Figure 1 shows the global emissions of <u>Co₂CO2</u> emission by sector. In order to mitigate global climate change concern, researchers in the past made an attempt to capture and sequestrate the emission of Co₂ before it released into the atmosphere. This approach would capture Co₂ from large sources, such as unmineable coal seams, saline formations, depleted oil and gas fields. alleviate the effects of global warming caused by the emission of carbon dioxide, it is necessary to capture and store

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the gas before it is released into the atmosphere. <u>Several There are several technologies such as chemical⁵</u>, and physical absorption⁶, biological⁷ and geological sequestration, and catalytic conversion that can be are applied for <u>Co₂</u> Carbon Dioxide sequestration sequestration. or the capture and storage of Carbon Dioxide. They are Chemical Absorption of Carbon Dioxide,⁵ Physical Absorption of Carbon Dioxide,⁶ Biological Sequestration of Carbon Dioxide,⁷ Geological Sequestration of Carbon Dioxide8 and Catalytic Conversions of Carbon Dioxide.⁹

Despite several technologies, Mmembrane separation is one of the key chemisorptions processes. used for the capture and sequestrationstorage of Co₂ carbon dioxide.¹⁰ The membrane processes used include membrane gas-separation,¹¹ and sequestration through membrane contactors¹², <u>etc.</u> Several researchers in the past A lot of researchers have carried out Co₂Carbon Dioxide sequestration using polymer membranes due to its reliability, scalability, easy operation and low costs membranes¹³.because the membranes are easy to operate and give reliable performances. Moreover polymeric membranes are easy to scale up and are low cost membranes, thus making them desirable among many.¹³ In comparison to other conventional technologies, Mmembrane contactors are advantageous compared to other conventional technologies because of their high interfacial contact area, their ability to withstand unlimited load, and enablinged mass transfer free of dispersion.¹⁴ Polymeric hollow fiber membrane contactors have been used by R-Naim et al (2012) for stripping Co, Carbon Dioxide-using diethanolamine solution.¹⁵ However, But fouling of polymeric membranes wasis common that lead to leading to low flux through the membrane. In addition, T the polymeric membranes lack sufficient mechanical strength and are mostly hydrophobic in nature.¹⁶ Due to these limitations, Because of these disadvantages, other types of membranes and membrane contactors were considered for effective sequestration of $Co_2Carbon$ Dioxide. Ceramic membrane contactors_are found to be cost effective, and have withstand very high temperature, pressure, and high chemical stability, and high-durability. As a result, the probability of corrosion was less and resists they do not corrode easily and can resist very high temperatures, -and pressures and strong chemicals. They are an excellent alternative to polymeric membranes when it comes to Co2 Carbon Dioxide capture.¹⁷

<u>Given this advantage</u>. In the present study the aim of this study was to investigate ,-the efficiency of a ceramic membrane contactor to capture $Co_2Carbon - Dioxide$ by the phenomenon of physical absorption is tested. The<u>is study aimed to</u> -aim of the work is to prepare a <u>water saturated with Co_2</u> (medium saturated), which has medium saturated with Carbon Dioxide. Water saturated with Carbon Dioxide has several useful applications. For example, carbonated water injected into oil ameliorates oil Materials used and Apparatus description

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Water from various sources was used for the experiment: a) Tap water taken from CGCRI, b) Milliq water with a resistance of 18.2 Ω taken from CGCRI laboratory, c) simulated sea water prepared in the CGCRI laboratory-Ggas containing 99.9% Carbon Dioxide and 99.9% Nitrogen is purchased from BOC. Table 1 showshow the weight compositions and physical characteristics of water used in the study while . The schematic diagram for the e experimental setup is xperimental set up is was shown in Figure 1. The gas-liquid contactor module made of tubular ceramic membrane (three in number) in line is-was connected to a feed water tank with a capacity of 2.5 liters and a pump which is was fitted for circulating feed through the membrane module. The flow rate through the magnetic drive chemical process pump is-was 750 ml/min. The ceramic membranes are made from 80% and 20% clay, m 80% alumina with an -and 20% clay and they have an outer (O.D) -and inner diameter (O.D.) of 10 mm and an inner diameter (I.D.) of and 7 mm respectively. The average pore size of the membranes iwass 0.5 to 1.5 micron with . The membranes have a contact area of 5.3298*103 mm² and a and a packing density of 41.52443 m_i^2/m_i^3 (total contact surface of the moduleace area /total volume of module). Effective length of each membrane iswas 125.6 mm, and thickness of the wall of each membrane iswas 2.58 mm and the -The-total volume of the module iswas 152435.6 mm3. The membranes are manufactured by the Central Glass and Ceramic Research InstituteCGCRI.

A display of the experimental set-up used and details of the apparatus are shown in Figure 2. A source line from gas cylinders <u>that</u> constitutes pressure reducer valves, pressure gauge, flow meters and <u>is are</u> connected to a mixing chamber <u>in turn</u> <u>which is connected</u> to the membrane module. The feed tank made of stainless steel has a rectangular cubic structure with a capacity of 2.5 liters. It is connected to the membrane module and a magnetic drive chemical process pump. The two ends of the three-membrane Perspex cylindrical module are connected to the feed tank and pump respectively.

Method

The experiment <u>is-was</u> carried out with milli-q water, tap water from CGCRI, Dhakuria lake water, Ichamati river water and simulated sea water. The simulated sea water <u>is-was</u> prepared in CGCRI laboratory by mixing 3.5 % sodium chloride with milli-q water. The feed tank <u>is-was</u> filled with 2.2 liters of feed (for each type of water) and <u>. The feed is</u> circulated at 750 ml/min through the tube side of the module via the magnetic drive chemical pump. Simultaneously CO₂ Carbon Dioxide gas (15%, 20% and

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100% $\underline{CO_2}$ Carbon Dioxide in a mixture of $\underline{CO_2}$ Carbon Dioxide and Nitrogen gas)_iswas passed through the shell side at the rate of 200 ml/min. The partial pressure of $\underline{CO_2}$ Carbon Dioxide in the gas mixture is was_0.10 Kg/cm2. For each type of water, samples are collected at regular intervals of time and the various parameters such as pH, conductivity, turbidity, TDS, and alkalinity etc. areare measured. The total dissolved Carbon DioxidCO₂ e in the aqueous solution wasis calculated by sample titration with titrating the samples with sodium hydroxide to estimate and the amount of estimating the amount of HOCO₂⁻ ions



Figure 2

Characterization of tubular ceramic membrane elements

Tubular ceramic membranes with 10mm od-<u>OD</u> 7mm id $\frac{1}{2}$ used in this <u>CO₂ earbon dioxide</u> capture sequestration experiments. Characterizations of these elements are done by XRD, FESEM, Chemical analysis and porosity, and pore size distributions,

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